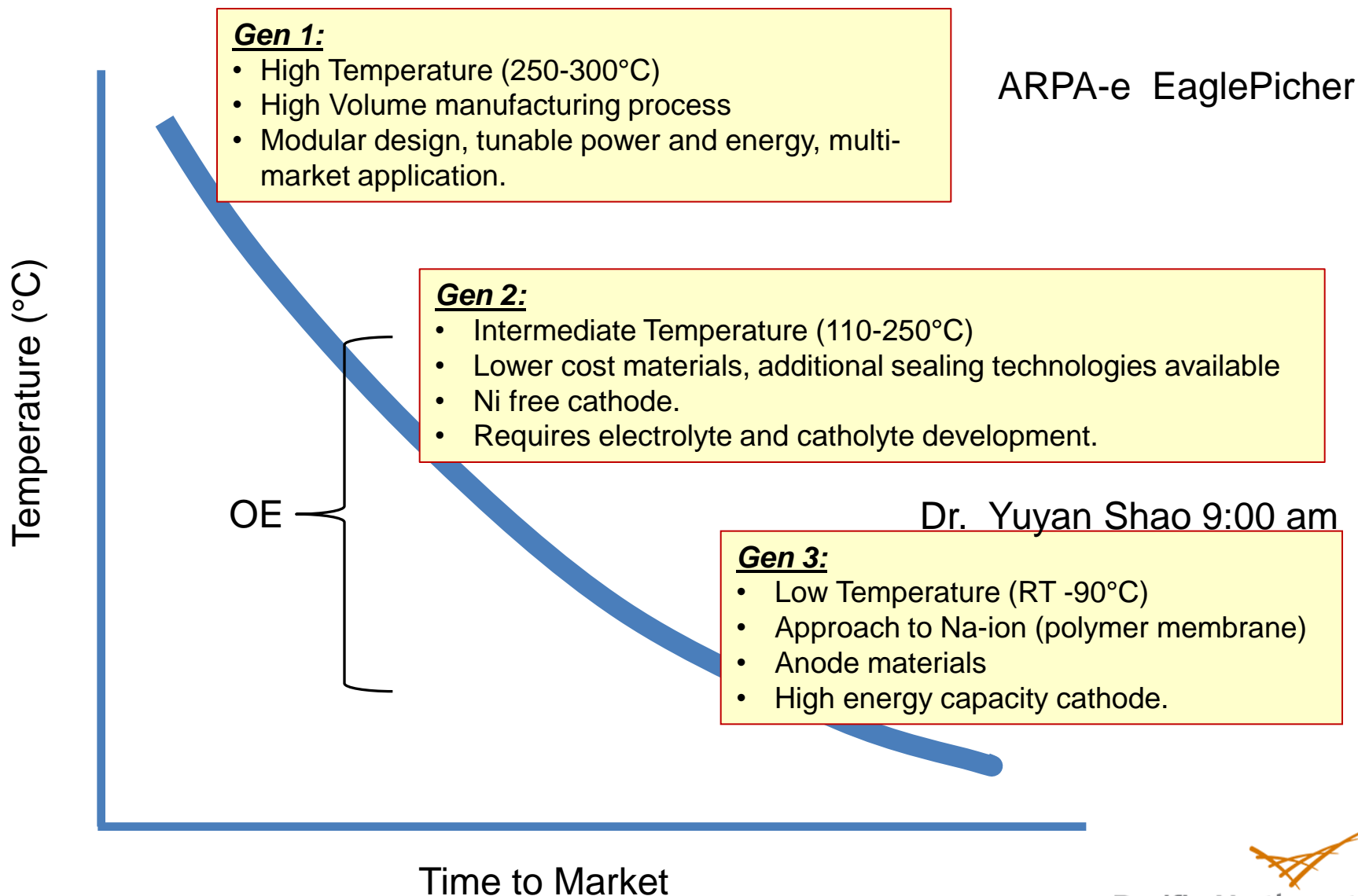


Na-Battery Development at PNNL

- ▶ Vincent Sprenkle, John Lemmon, Xiaochuan Lu, Guosheng Li, Jun Cui, Jin Yong Kim, Brent Kirby, Nathan Canfield, Dave Reed, Eric Mast, Richard Pearson, Kerry Meinhardt, Jeff Bonnett, Greg Coffey, Jirgal Mansonav.
- ▶ EaglePicher ARPA-e team: Dave Lucero, Bob Higgins, Jim DeGruson, Julie Baumann, Eric Raub, Rebecca Cragan, Charlie Huddleston.

Progression of Planar Sodium Battery Technology



Acknowledgements

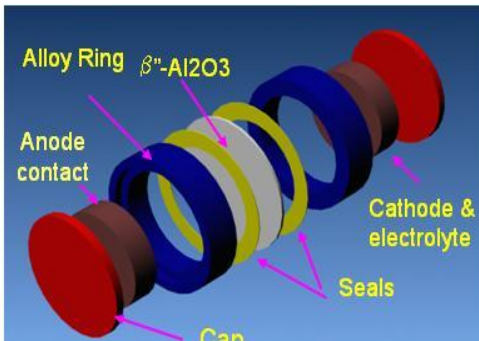
- **ARPA-e DOE Award Number: DE-AR0000045**
 - *Dr. Mark Johnson, Dr. Dave Danielson*
- **DOE-OE Energy Storage Program,**
 - *Dr. Imre Gyuk*
- **PNNL internal LDRD Funding**

EaglePicher Technologies- PNNL

Planar Na-Beta Batteries Development for Renewable Integration and Grid Applications

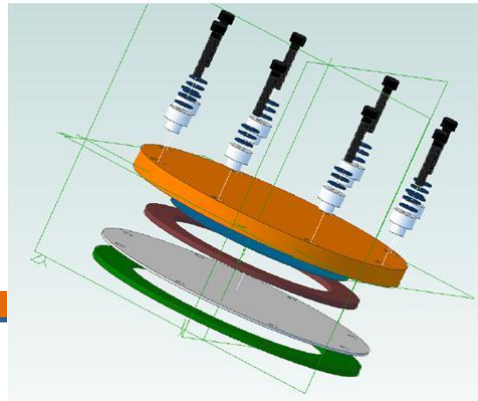
Eagle-Picher/PNNL Path to Planar Na Battery

3.0cm² Button Cell



Materials development and performance testing.

64cm²
XL-Button Cell

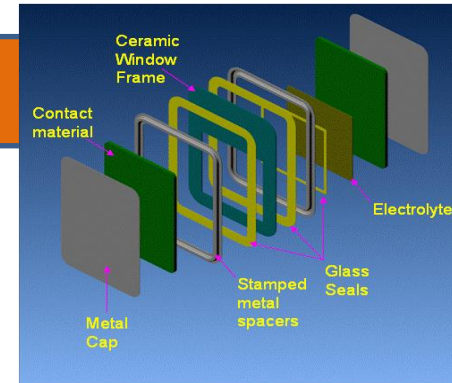


Materials scale-up with large-scale performance and life testing.

- *Tubular Na –Metal Halide chemistry demonstrated > 1000 cycles at high DOD.*
- *Decrease capital cost by moving to high volume planar manufacturing. Planar technology has higher volumetric power density than tubular architecture*
- *Increase cycle life by reduced temperature operation.*

➤ *3 year program to scale up and demonstrate planar Na-battery technology.*

Multicell
Planar Stack



Manufacturing friendly components and fabrication techniques.

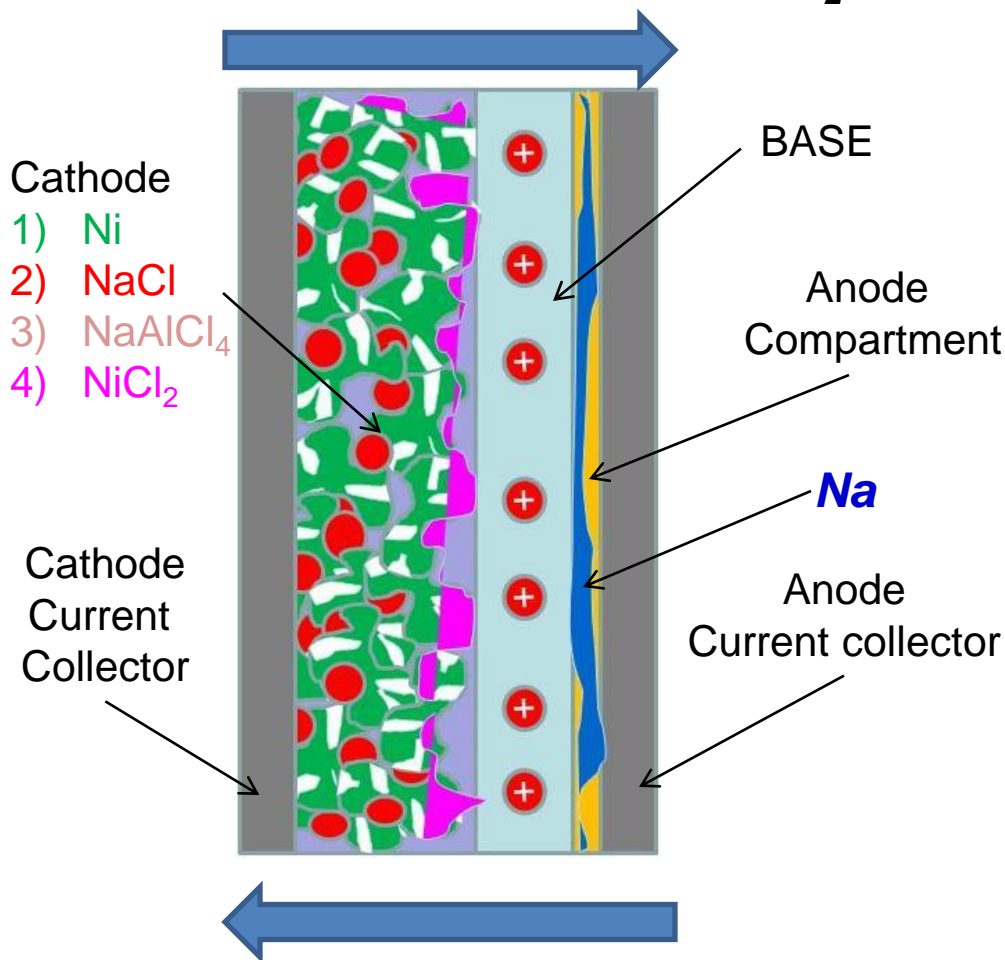
200cm² Stack



Modular stack design with performance and life testing.

Basic Na-NiCl₂ Battery Chemistry

Charging Reaction



Discharging Reaction



Key elements

- 2.58 V OVC
- ~3.0 V cutoff voltage for charging
 - Increase R from NiCl₂
 - Melt degradation.
- 1.8 V cutoff on discharging
 - Al plating from melt
- Typically 20 – 80% SOC swing.

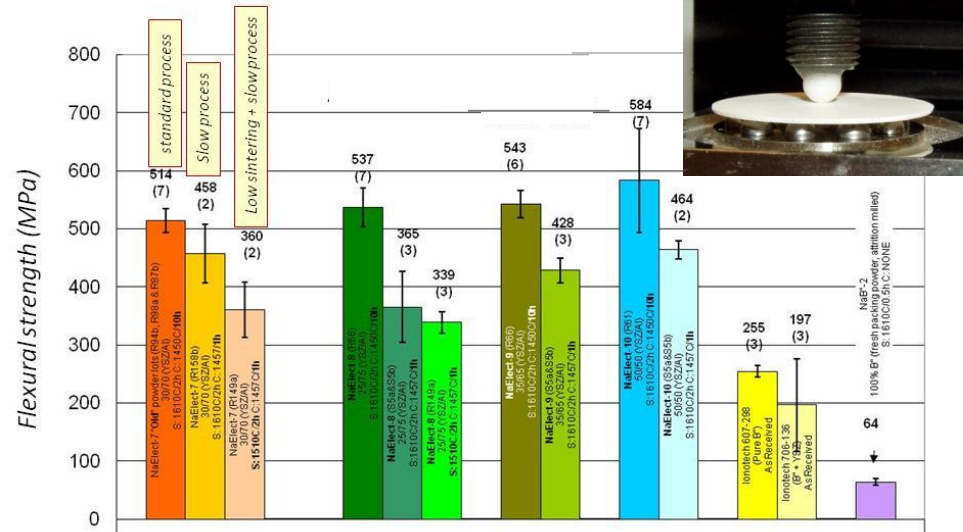
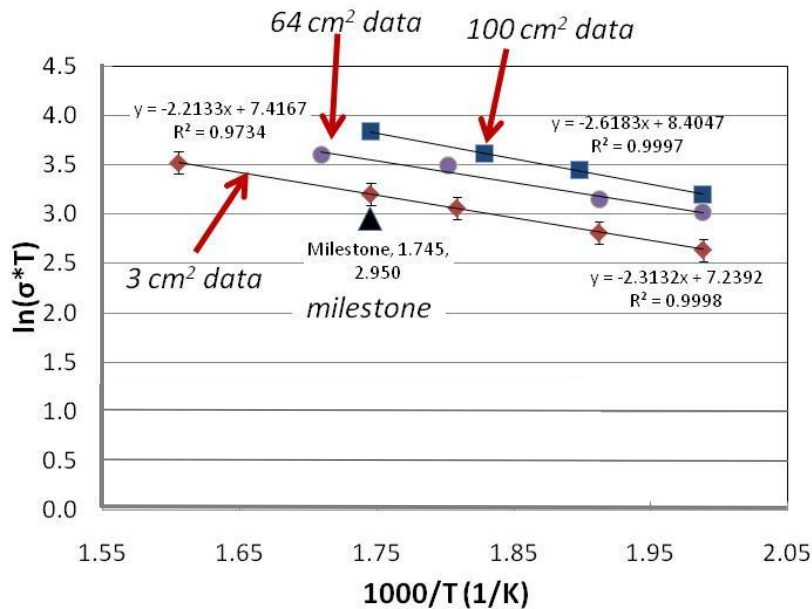
PNNL efforts focused on

- Scale-up of BASE fabrication process.
- Development of durable glass seals capable of withstanding melt
- Demonstrating larger scale 64 cm² cells
- Cathode chemistry development to improve durability at higher specific energy density.
- Transition technology to EP

BASE properties are function of fabrication, composition, and processing conditions.

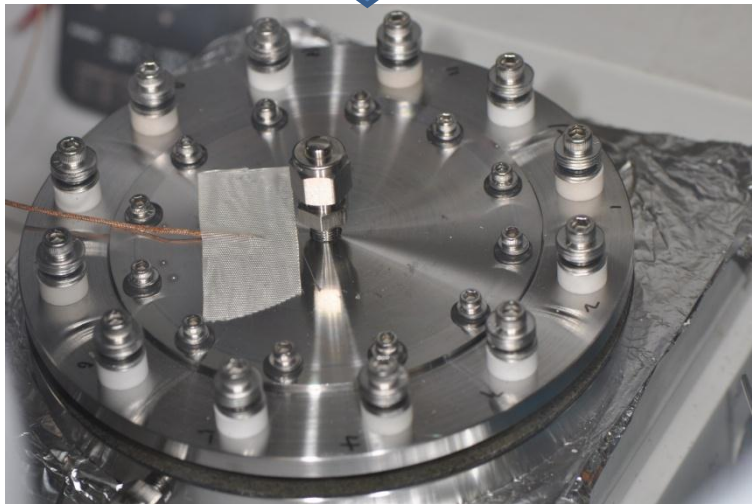


64 cm² BASE sample glass sealed to a alumina ring prior to application of electrodes and resistivity test.



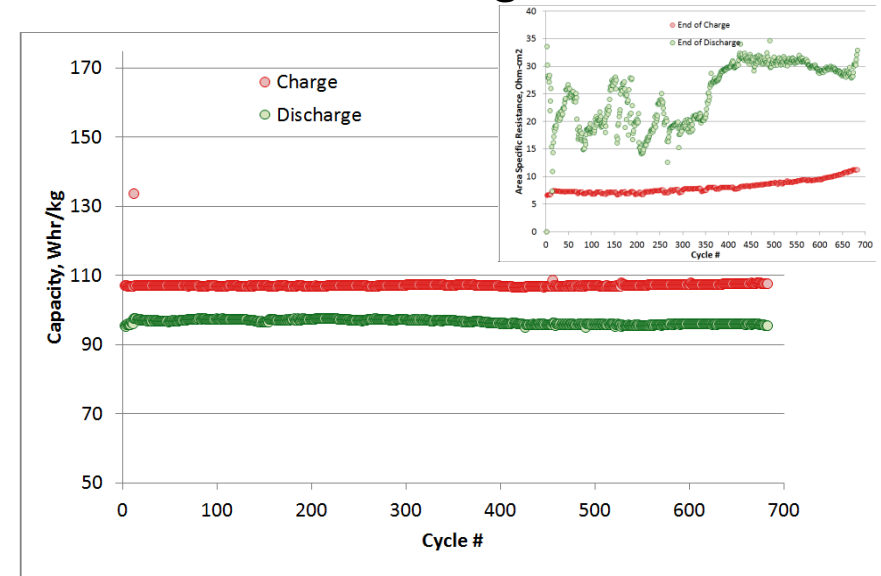
- Critical to understand impact of process conditions on flexural strength and conductivity.
- Goal : Maintain > 0.03 S/cm at 300 ° C with RT flexural strength > 400 MPa flexural strength.

Progress of 64 cm² cell

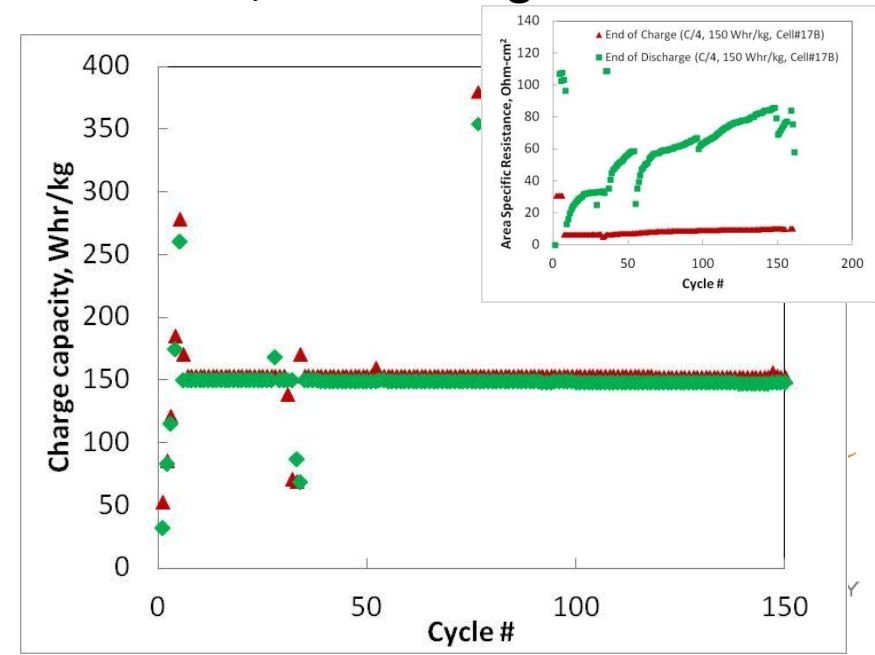


- 64cm² cell - 100whr/kg at 1C - 91% efficiency - 280°C for over 700 cycles
- No capacity fade for first 800 cycles .

64cm² cell, 100 Whr/kg at 1C - 280°C

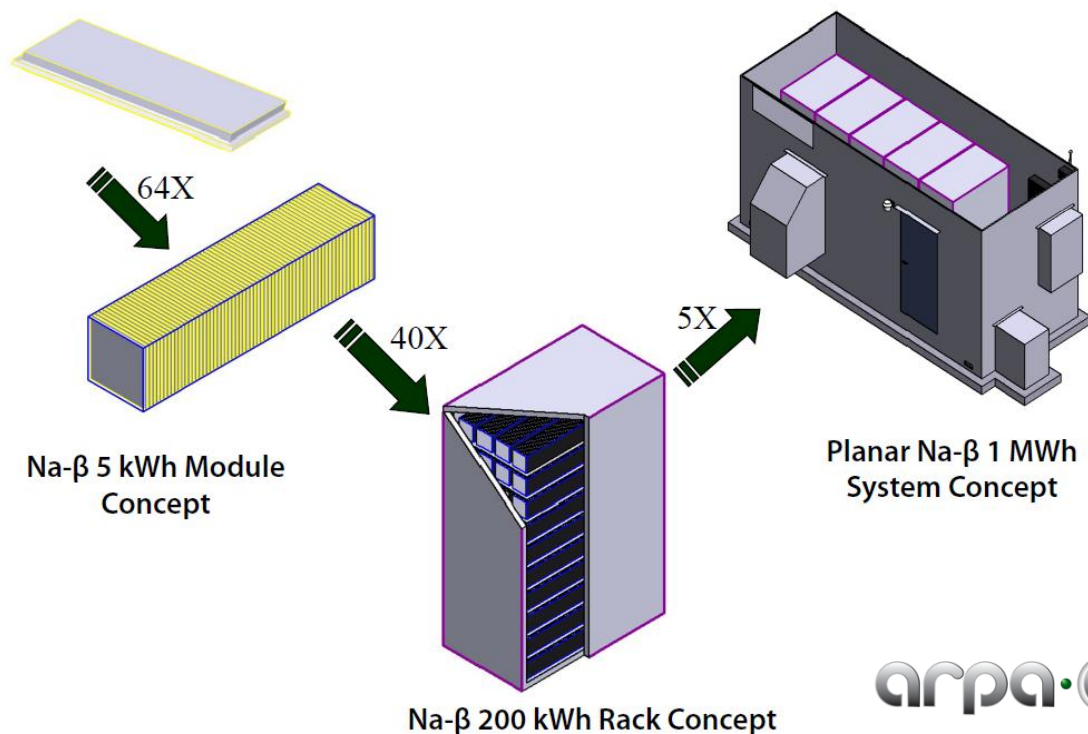


64cm² cell, 150 Whr/kg at C/4 - 280°C

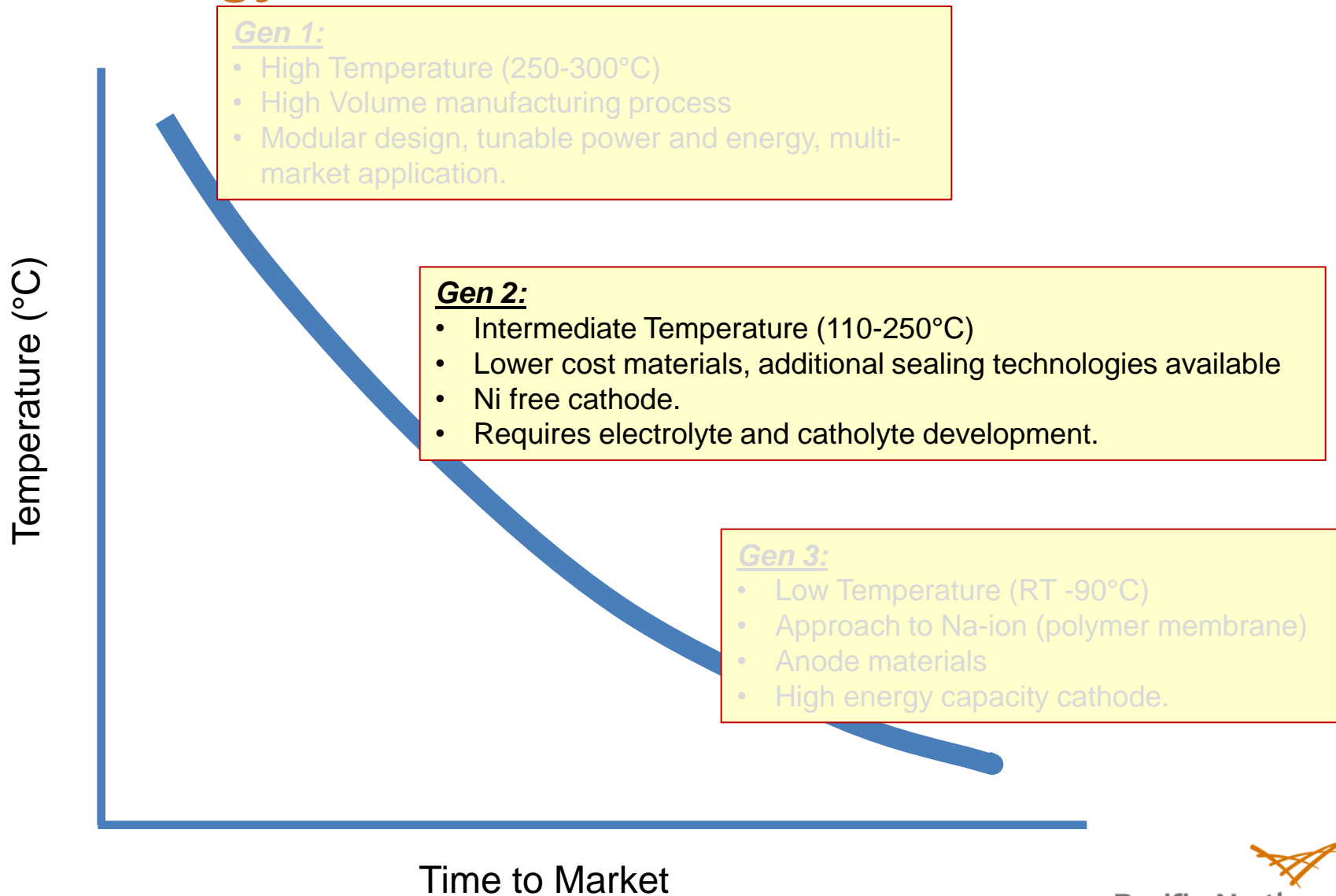


EaglePicher – PNNL Next Steps

- Assemble and test multicell 64 cm² stack – 150 Whr/kg of active cathode
- 1000 hrs durability of seal
- Larger scale cells running at 200 Whr/kg of active cathode.
- 5 kW module



Intermediate Temperature Sodium Battery Technology



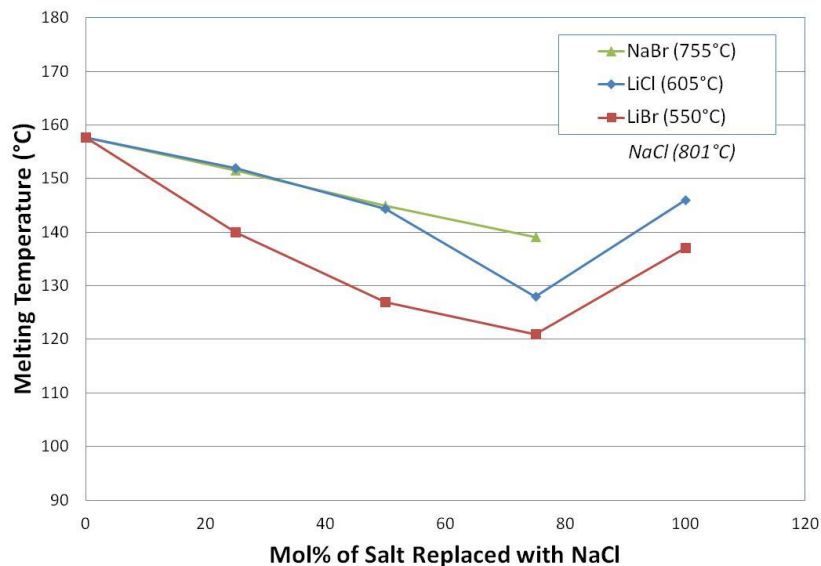
FY11 Intermediate Temperature (110-250 °C) Na-Metal Halide Battery Research Plan

- **Goal:** To demonstrate Na- metal halide battery operated at $\leq 200^{\circ}\text{C}$
 - *64 cm² cell with comparable performance compared to current cells operated at 280 °C*

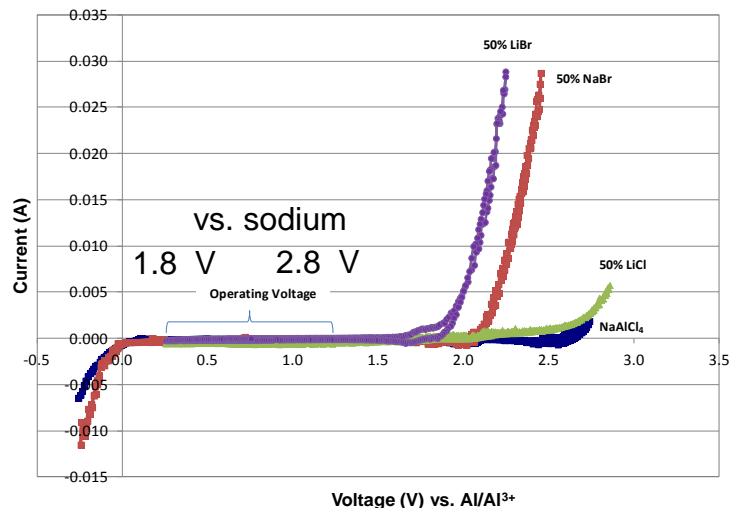
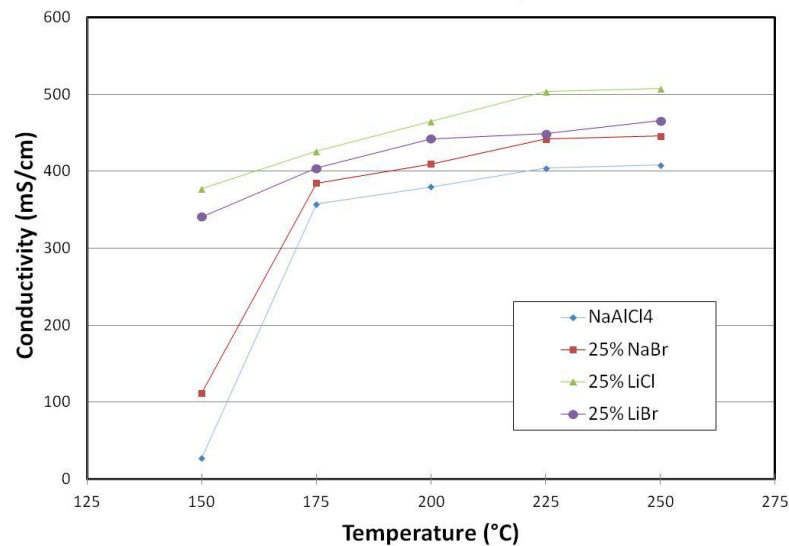
- **Technical Challenges**
 - *Catholyte and Cathode Chemistry*
 - *Low-resistance BASE*
 - *Na wetting at lower temperatures*
 - *Seal and new cell design*

Low Temperature Catholyte Development

Melting Temperature of NaAlCl_4 Catholyte



Ionic Conductivity

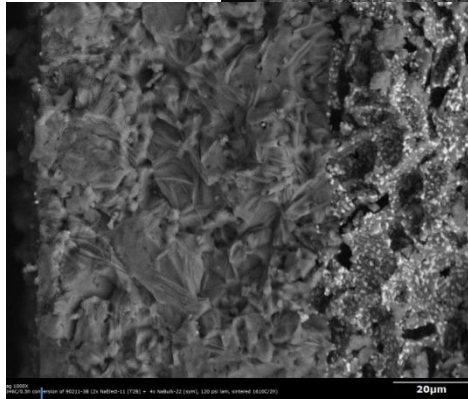
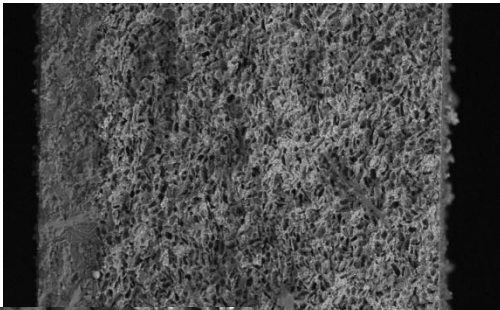


Additions to NaAlCl_4

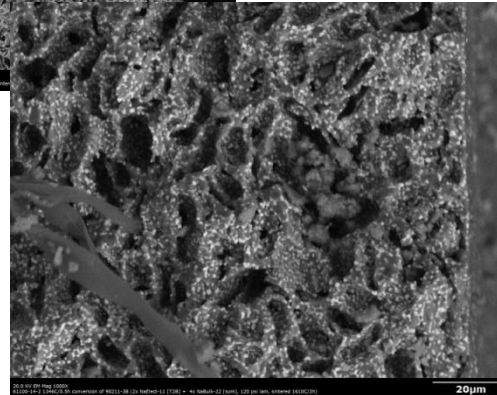
- Decrease T_m of catholyte by 20 - 40°C
- High ionic conductivity < 200°C with $\geq 25\%$ salt replacement.
- Does not impact electrochemical stability of catholyte.

Low Temperature BASE Development

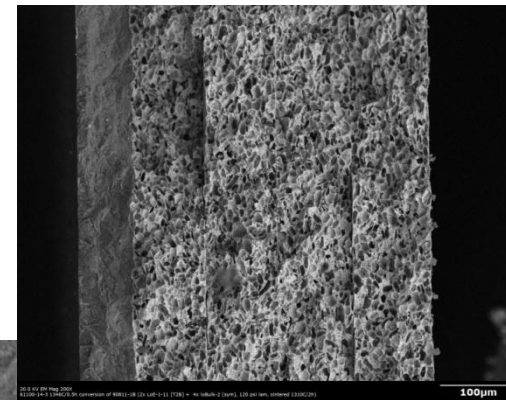
*Sinter 1600°C
Convert 1350°C*



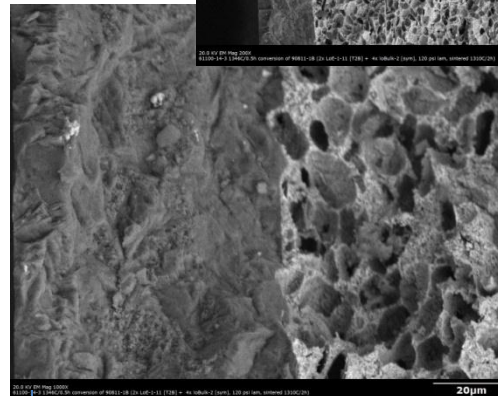
Electrolyte –
50 µm - (100% β'')



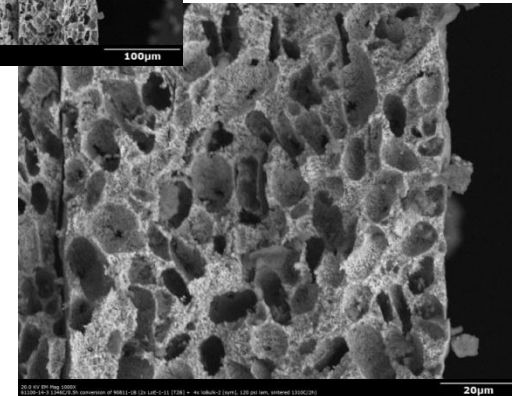
Porous Electrode
~400µm (70/30 β'' – YSZ)



*Sinter 1400°C
Convert 1350°C*



Electrolyte –
50 µm - (100% β'')

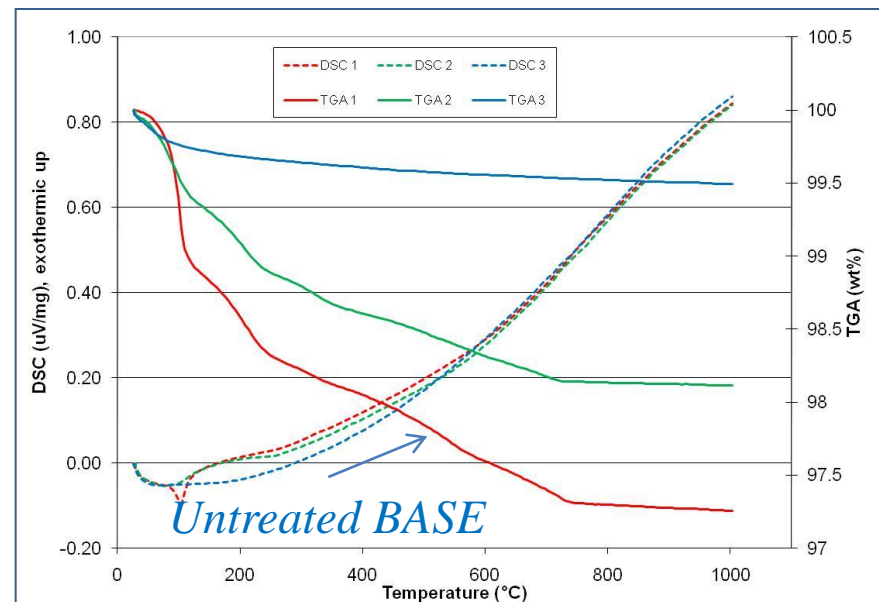


Porous Electrode
~400µm (70/30 YSZ - β'')

- Goal is to minimize electrolyte resistance while retaining sufficient strength for larger scale planar batteries.
- 50 µm β'' electrolyte on porous support
- Currently focused on determining strength – porosity relationship.

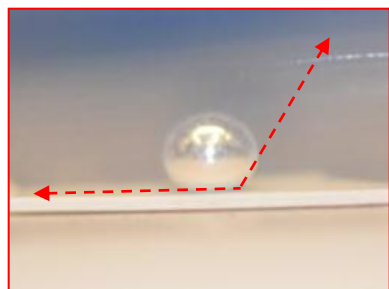
Low Temperature Na wetting

- As-prepared BASE shows extensive hydration after exposure to air. Wetting angle $> 90^\circ$ for all temperatures studied and poor adherence.
- Vacuum treated BASE shows improved wetting and adherence
- Wetting angle $> 130^\circ$ at 250°C - significant issues for low temperature operation?



Na drop showed no adherence to β'' surface
 \rightarrow Na rolled off surface
 $\theta \sim 180^\circ$

$T = 250^\circ\text{C}$

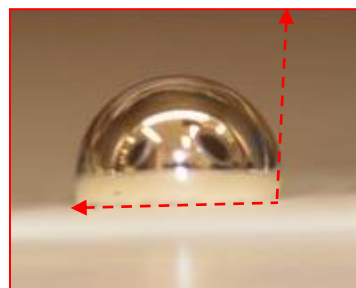


$\theta \sim 130^\circ$

Treated BASE
 $425^\circ\text{C} - 60 \text{ hr vacuum}$

Na drop showed no adherence to β'' surface
 \rightarrow Na rolled off surface
 $\theta \sim 180^\circ$

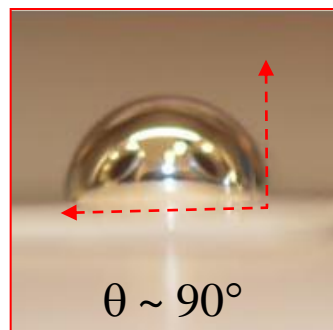
$T = 300^\circ\text{C}$



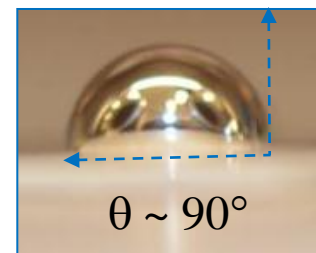
$\theta \sim 100^\circ$

Na drop showed no adherence to β'' surface
 \rightarrow Na rolled off surface
 $\theta \sim 180^\circ$

$T = 325^\circ\text{C}$

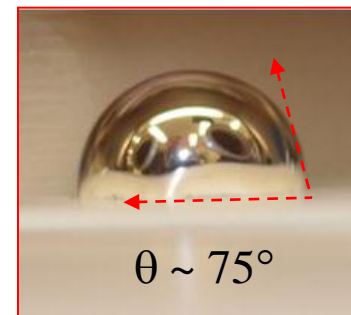


$\theta \sim 90^\circ$



$\theta \sim 90^\circ$

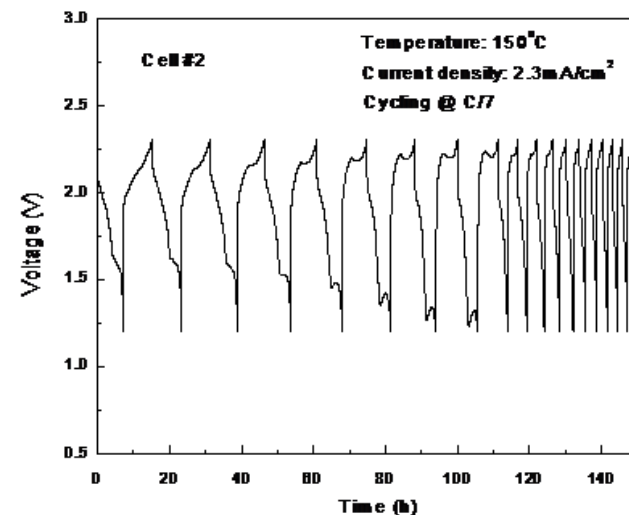
$T = 350^\circ\text{C}$



$\theta \sim 75^\circ$

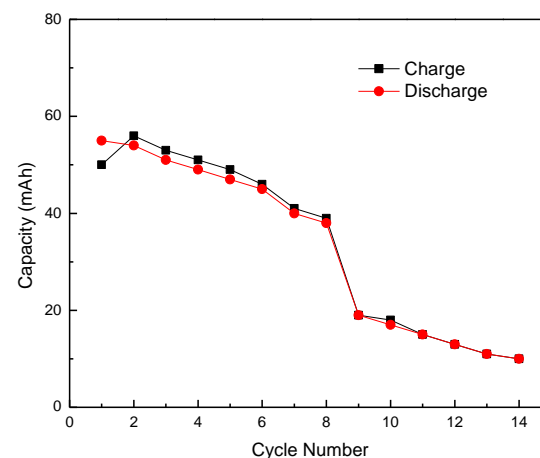
Intermediate Temperature Na-S

- **Goal:** Develop 150 – 200°C temperature Na – S battery which can:
 - Less corrosive environment
 - Built in discharge state and charged on site
 - Can withstand multiple freeze/thaw cycles.



Sulfur Solubility in Various Organic Solvents (wt.%)

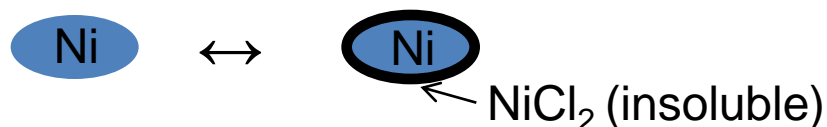
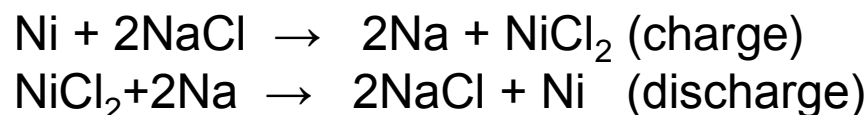
	Boiling point (°C)	25°C	50°C	100°C	150°C	200°C
tri(ethylene glycol) dimethyl ether	216	-----	0.5	2.5	7.0	-----
tetra(ethylene glycol) dimethyl ether	275	0.16	1.01	3.0	7.0	-----
di(ethylene glycol) dibutyl ether	256	-----	-----	0.5	1.5	-----
Dimethylaniline	194	3.37	6.92	38.4	-----	-----
propylene carbonate	242	-----	-----	-----	-----	-----
ethylene carbonate	244	-----	-----	-----	-----	-----



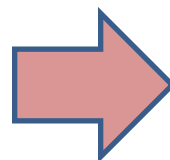
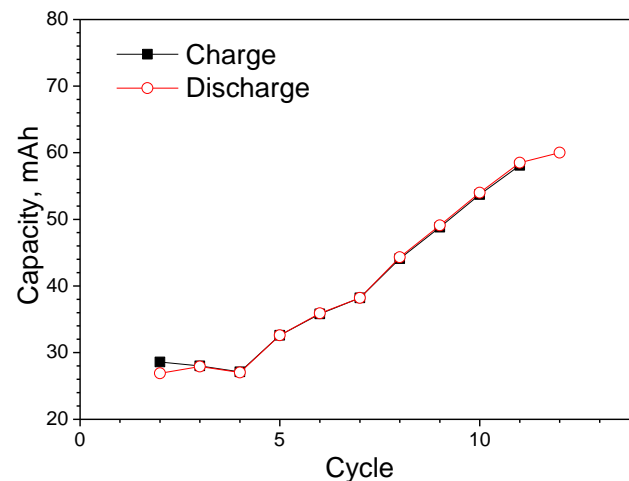
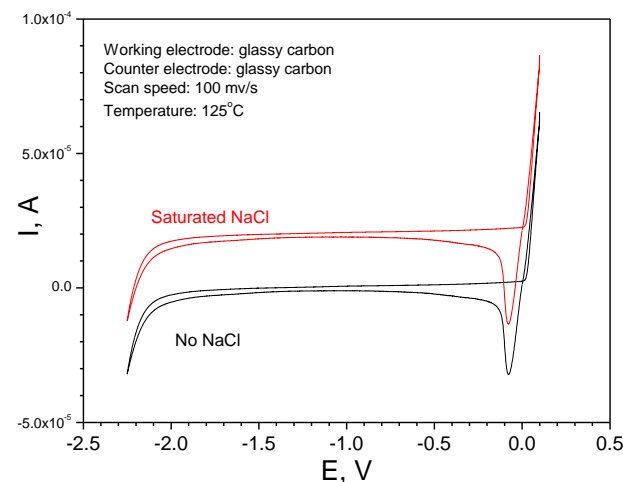
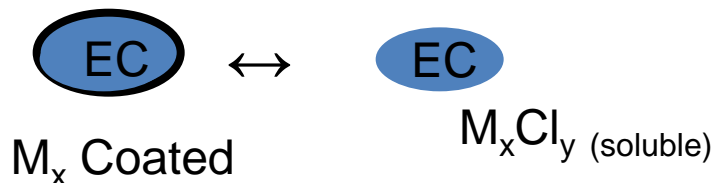
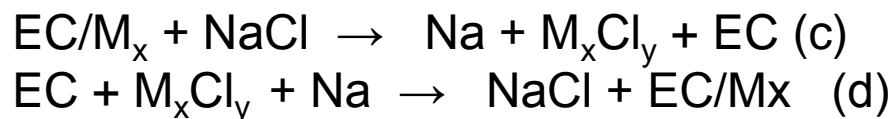
Na-Metal Halide Concepts (non-Ni)

- Goal: Replace highest cost material component(Ni) with lower cost metals with improved performance.

ZEBRA type chemistry: insoluble MH



Metal coated chemistry: soluble MH

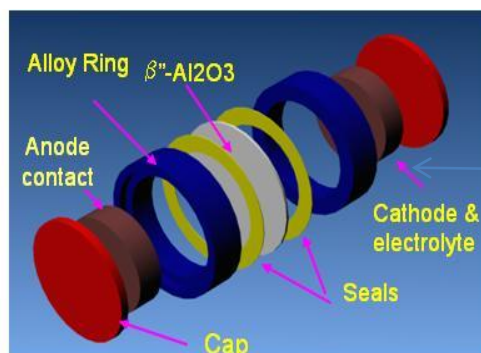


Intermediate Temperature Na-Air with BASE

Goal: Improve performance, low cost alkali metal – air.

Path: Improve solubility of Na_xO_y products in cathode with higher temperature.

3.0cm² Button Cell



Replace metal cathode with temperature stable air cathode.

Cell Characteristics:

Temperature: 140°C

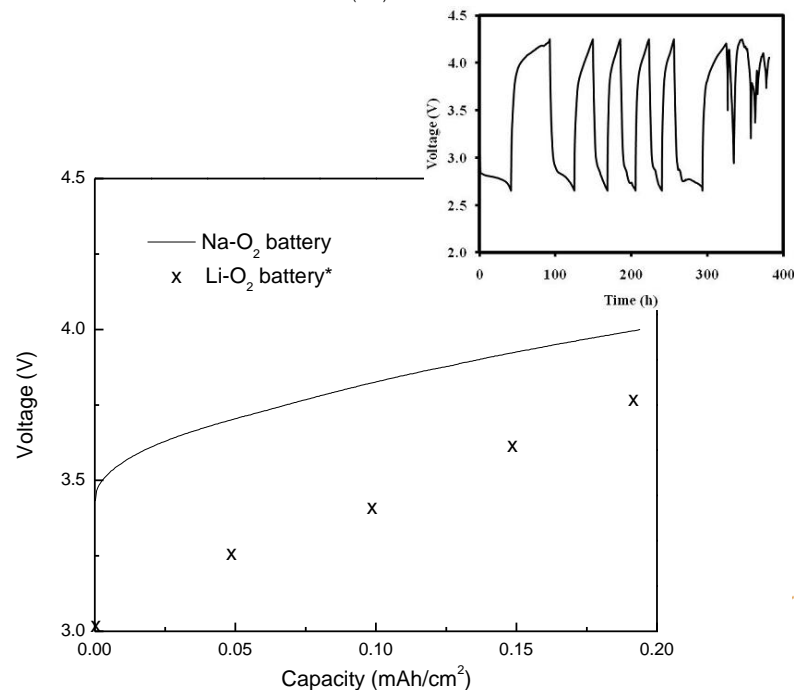
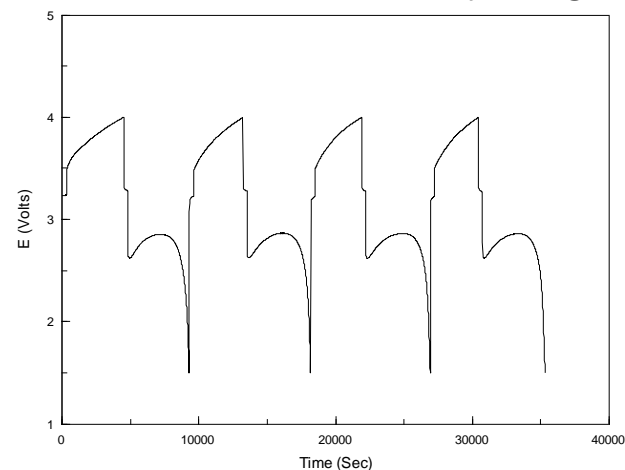
OCV: 3.2V vs Na

Current: 0.15mA/cm².

Summary:

- High IR from BASE electrolyte.
- Cycled in air, capacity decreases.
- Overpotential on charge higher than Li.
- Overpotential increase rate lower than Li.

Na-Air Low rate cycling



* J. Xiao, et al., J. Power Sources 196 (2011) 5674

NATIONAL LABORATORY

Acknowledgements

- **ARPA-e DOE Award Number: DE-AR0000045**
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- **DOE-OE Energy Storage Program,**
 - *Dr. Imre Gyuk*
- **PNNL internal LDRD Funding**